AMENDMENTS TO THE CLAIMS:

This listing of Claims will replace all prior versions, and listings, of Claims in the application:

Listing Of Claims:

Claim 1 (Currently Amended) A process for hydroprocessing a heavy hydrocarbon oil, comprising contacting a heavy hydrocarbon oil in the presence of hydrogen with a mixture of hydroprocessing catalyst I and hydroprocessing catalyst II wherein catalyst I comprises a Group VIB metal component and optionally a Group VIII metal component on a porous inorganic carrier, said catalyst having a specific surface area of at least 100 m^2/g, a total pore volume of at least 0.55 ml/g, and a pore size distribution for inhibiting sediment formation and promoting asphaltene removal such that at least 50% of the total pore volume in pores with a diameter of at least 20 nm (200 Å) and at least 65% of the total pore volume in pores with a diameter of 10-120 nm (100-1200 Å), wherein less than 25% of the total pore volume of catalyst I is in pores having a diameter of 10 nm (100 Å) or less, and

catalyst II comprises a Group VIB metal component and optionally a Group VIII metal component on a porous inorganic carrier, said catalyst having a specific surface area of at least 100 m^2/g, and a pore size distribution for providing catalytic activity and inhibiting sediment formation such that a total pore volume of at least 0.55 ml/g, 30-80% of the pore volume in pores with a diameter of 10-20 nm (100-200 Å), and at least 5% of the pore volume in pores with a diameter of at least 100 nm (1000 Å), wherein less than 25% of the total pore volume of catalyst II is in pores having a diameter of 10 nm (100 Å) or less, and

with catalyst I having a larger percentage of its pore volume in pores with a diameter of at least 20 nm (200 Å) than catalyst II.

2. (Original) The process of claim 1 wherein the carrier of catalyst I consists essentially of alumina and/or wherein the carrier of catalyst II consists essentially of alumina and at least 3.5 wt.% of silica, and/or wherein catalyst II comprises 0.1-2 wt.% of a Group IA metal component.

3. (Original) The process of claim 1 wherein catalyst II has less than 50% of its pore volume in pores with a diameter of at least 20 nm (200 Å).

4. (Original) The process of claim 1 wherein catalyst I and/or catalyst II comprise 7 to 20 wt.% of a Group VIB metal component, calculated as trioxide on the weight of the catalyst, and 0.5 to 6 wt.% of a Group VIII metal component, calculated as oxide on the weight of the catalyst

5. (Original) The process of claim 1 wherein the heavy hydrocarbon feed is a feed of which at least 50 wt.% boils above 538°C (1000°F) and which comprises at least 2 wt.% of sulfur and at least 5 wt.% of Conradson carbon.

6. (Original) The process of claim 1 which is carried out in an ebullating bed.

7. (Currently Amended) A mixture of catalysts comprising a
catalyst I which comprises a Group VIB metal component and optionally a Group VIII metal component on a porous inorganic carrier, and 0.5 to 6 wt.% of a Group VIII metal component, calculated as oxide on the weight of the catalyst, on a porous inorganic carrier, said catalyst having a specific surface area of at least 100 m^2/g, a total pore volume of at least 0.55 ml/g, and a pore size distribution for inhibiting sediment formation and promoting asphaltene removal such that at least 50% of the total pore volume in pores with a diameter of at least 20 nm (200 Å) and at least 65% of the total pore volume in pores with a diameter of 10-120 nm (100-1200 Å), wherein less than 25% of the total pore volume of catalyst I is in pores having a diameter of 10 nm (100 Å) or less, and a
catalyst II which comprises a Group VIB metal component and optionally a Group VIII metal component on a porous inorganic carrier, said catalyst having a specific surface area of at least 100 m^2/g, a total pore volume of at least 0.55 ml/g, and a pore size distribution for providing catalytic activity and inhibiting sediment formation such that 30-80% of the pore volume in pores with a diameter of 10-20 nm (100-200 Å), and at least 5% of the pore volume in pores with a diameter above 100 nm (1000 Å), wherein less than 25% of the total pore volume of catalyst II is in pores having a diameter of 10 nm (100 Å) or less, and
with catalyst I having a larger percentage of its pore volume in pores with a diameter of at least 20 nm (200 Å) than catalyst II.

8. (Original) The catalyst mixture of claim 7 wherein the carrier of catalyst I consists essentially of alumina and/or wherein the carrier of catalyst II consists essentially of alumina and at least 3.5 wt.% of silica.

9. (Original) The catalyst mixture of claim 7 wherein catalyst II has less than 50% of its pore volume in pores with a diameter above 200 Å.

10. (Original) The catalyst mixture of claim 7 wherein catalyst I and/or catalyst II comprise 7 to 20 wt.% of a Group VIB metal component, calculated as trioxide on the weight of the catalyst, and 0.5 to 6 wt.% of a Group VIII metal component, calculated as oxide on the weight of the catalyst.